

# Stochastic modeling of transient boundary layers in high-Rayleigh-number thermal convection

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## Introduction

- **Turbulent thermal convection** denotes the chaotic flow in a layer of fluid that is driven by buoyancy forces due to an unstable temperature stratification. The flow becomes turbulent when buoyancy and inertial forces are much larger than viscous forces. This type of flow is encountered in numerous applications that range from technical to atmospheric and astrophysical scales (e.g. [1]).
- In a closed sample, **transient boundary layers** achieve the bulk-surface coupling (e.g. [2, 3]). These are mixed-type convective Blasius boundary layers (e.g. [4]) that control the achievable heat transfer (e.g. [5]).

## Main objectives

- Investigation of **transient boundary layers** in turbulent Rayleigh–Bénard convection.
- **Modeling** using a numerical tool applicable throughout the **relevant parameter space**.
- Capture **wall-normal transport processes** in mixed-type (Blasius-convective) boundary layers by utilizing a stochastic **one-dimensional turbulence** (ODT) model [6].

## Model formulation

The **ODT model** aims to **resolve all relevant scales** of a turbulent flow along a notional line-of-sight ('ODT line'). Flow variables are resolved along this line on a dynamically adaptive grid [7]. Instantaneous flow profiles are evolved by **deterministic diffusion** along the ODT domain, and a **stochastic process** that models the effects of turbulent advection, pressure fluctuations, and buoyancy forces that are aligned with the ODT domain ( $z$  coordinate) [6, 8, 9].

- **ODT equations** for Cartesian velocity components ( $u_i$ ) = ( $u, v, w$ ) and temperature  $T$  are [9]

$$\frac{\partial u_i}{\partial t} + \mathcal{E}_i(\alpha) = \nu \frac{\partial^2 u_i}{\partial z^2}, \quad \frac{\partial T}{\partial t} + \mathcal{E}_T = \kappa \frac{\partial^2 T}{\partial z^2},$$

where  $\nu$  is the kinematic viscosity and  $\kappa$  the thermal diffusivity.

- **Stochastic terms**  $\mathcal{E}_i$  and  $\mathcal{E}_T$  represent the effects of discrete turbulent **mapping** ('eddy') events in which the **triplet map** models the overturning motion of a turbulent eddy (Fig. 1).
- The **'eddy' rate**  $\tau^{-1}(\ell, z_0; t)$  of a size- $\ell$  'eddy' event at location  $z_0$  at time  $t$  depends on the **local total available energy** for the momentary flow state. The eddy rate is [8, 9]

$$\tau^{-1} = C \sqrt{\frac{2}{\rho_0 V \ell^2} (E_{\text{kin}} - E_{\text{pot}} - Z E_{\text{vp}})},$$

where  $\rho_0$  is the reference mass density,  $V = \ell^3$  the notional 'eddy' volume,  $E_{\text{kin}}$  and  $E_{\text{pot}}$  the local changes in the 'eddy' kinetic and potential energy, respectively, and  $E_{\text{vp}}$  is a viscous penalty energy that effectively suppresses unphysically small 'eddy' events below the viscous length scale [6].

- **Fixed ODT model parameters**  $C = 60$ ,  $Z = 220$ , and  $\alpha = 2/3$  are used here. Definitions are identical to [9], but we rely on the calibration performed in [10].

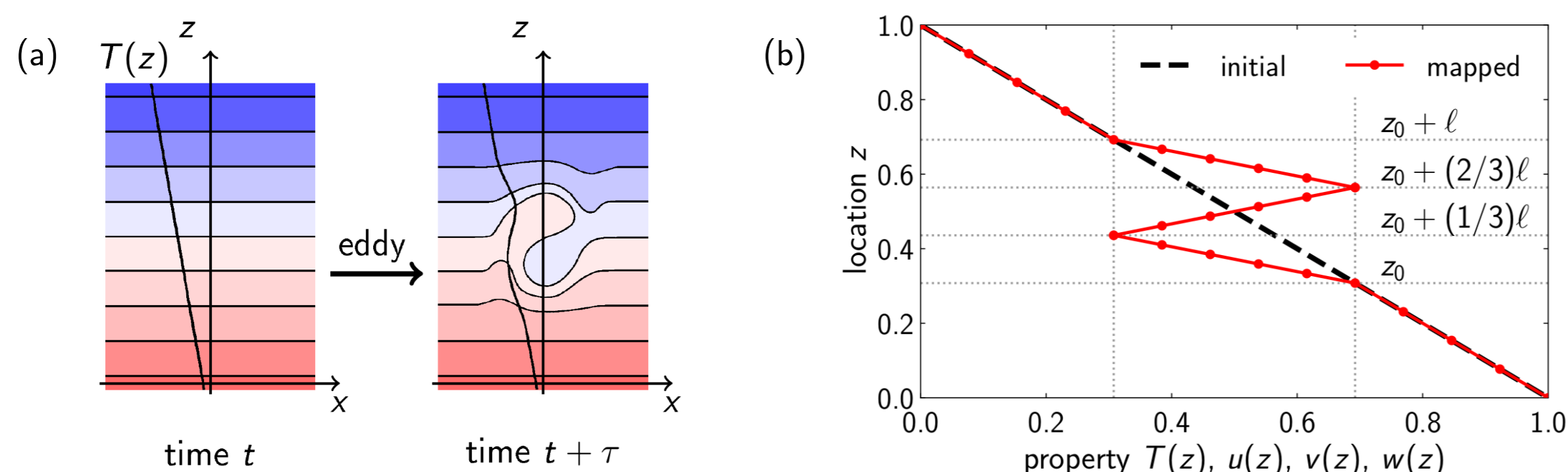


Figure 1: (a) Schematic of a notional 'eddy' turnover. (b) Triplet mapping in a turbulent 'eddy' event.

## Flow configuration and model application

- **Layer of fluid** of height  $L$  for which wall-normal transport is resolved by a vertical ODT line as sketched in Fig. 2(a)
- **Transient boundary layers** form over the heated and cooled wall as sketched in Fig. 2(b)
- **Uniform constant gravity**  $g = -g e_z$
- **Oberbeck–Boussinesq fluid**: linear equation of state,  $\rho(T) = \rho_0 [1 - \beta(T - T_0)]$ , where  $\beta$  denotes the thermal expansion coefficient and the subscript '0' the reference values
- **Smooth constant-temperature no-slip wall**: heated wall ( $T_{\text{hw}}$ ) at bottom  $z = 0$  and cooled wall ( $T_{\text{cw}}$ ) at top  $z = L$  with prescribed constant temperature difference  $\Delta T = T_{\text{hw}} - T_{\text{cw}}$
- The flow is characterized by the **Prandtl** ( $Pr$ ) and **Rayleigh** ( $Ra$ ) number that are fixed at

$$Pr = \frac{\nu}{\kappa} = 0.7 \quad \text{and} \quad Ra = \frac{g \beta \Delta T L^3}{\nu \kappa} = 3 \times 10^{10}.$$

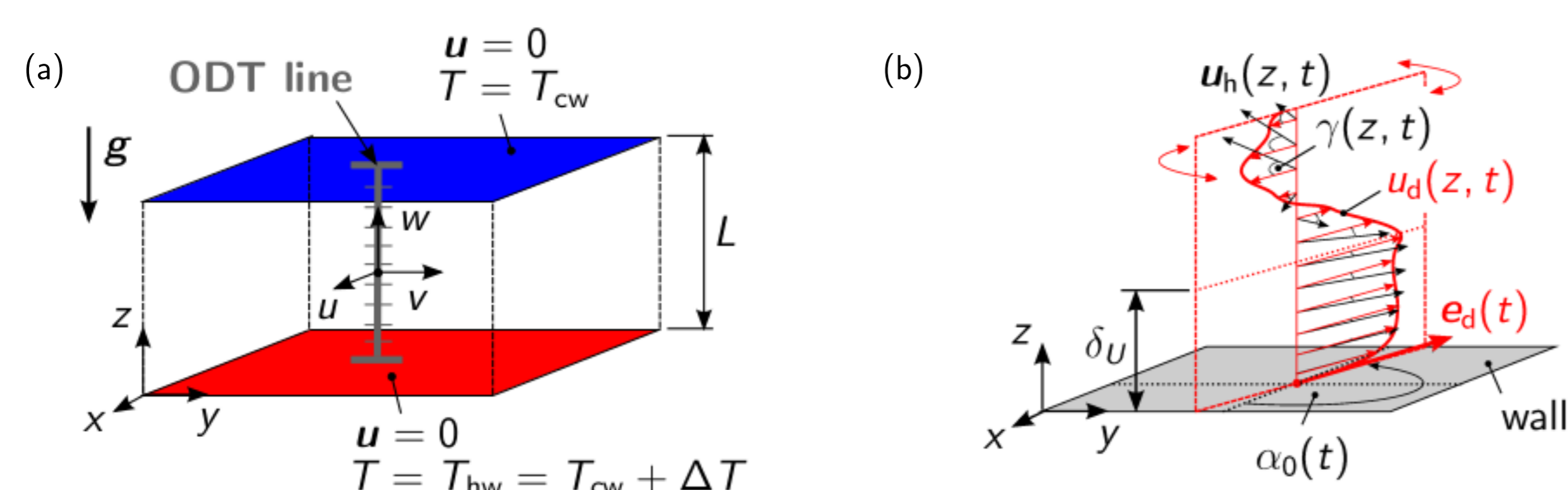


Figure 2: (a) Sketch of the canonical Rayleigh–Bénard set-up investigated. We focus on wall-normal transport far from the lateral walls (which are located at infinity) and resolve the flow only along a notional vertical 'ODT line'. (b) Sketch of the momentary local viscous boundary layer of thickness  $\delta_U$ . Here  $u_h = (u, v, 0)^T$  denotes the horizontal velocity vector,  $e_d$  the momentary boundary-layer 'downstream' direction,  $u_d$  the corresponding momentary 'downstream' velocity component,  $\alpha_0(t)$  the momentary wall-shear angle, and  $\gamma$  the local deviation angle between  $u_h$  and  $e_d$ .

## Transient boundary layers in thermal convection

- Fig. 3(a) shows the **normalized mean temperature**

$$\Theta(z) = (\langle T(z, t) \rangle - T_b) / \Delta T \quad \text{with} \quad T_b = (T_{\text{hw}} + T_{\text{cw}}) / 2,$$

where  $T_b$  is the bulk temperature that is here measured at the midplane  $z = L/2$ . Angle brackets  $\langle \cdot \rangle$  denote a conventional temporal average. **ODT captures the linear surface layer** and the **thermal log layer** (dashed green lines). The prefactor  $A$  in  $\Theta(z) = A \ln(z/L) + B$  is obtained with ODT and the reference direct numerical simulation (DNS) [11], but not the additive constant  $B$ .

- Fig. 3(b) shows the **root-mean-square (r.m.s.) fluctuation temperature**  $\sigma_T$ , which is obtained for  $\phi = T$  from the general formula

$$\sigma_\phi(z) = \sqrt{\langle \phi^2(z, t) \rangle - \langle \phi(z, t) \rangle^2}.$$

ODT and DNS [11] results have been normalized by their maximum value  $\sigma_T^{\text{max}}$ . This maximum is nominally expected as monomodal peak at  $z = \delta_T$  but ODT exhibits a bimodal peak due to missing fluctuations. This is a modeling artifact of the triplet map (Fig. 1) as shown in [7] for channel flow.

- Fig. 3(c) shows the **boundary-layer 'downstream' velocity**  $\langle u_d \rangle$  that is obtained by conditional averaging of the momentary projected velocity  $u_d(z, t)$ , where

$$u_d(z, t) = e_d(t) \cdot u(z, t) \quad \text{with} \quad e_d = (\tau_{xz} e_x + \tau_{yz} e_y) / \tau_w, \quad \tau_w = \sqrt{\tau_{xz}^2 + \tau_{yz}^2},$$

in which  $\tau_{xz}(t)$  and  $\tau_{yz}(t)$  are the horizontal ( $x, y$ ) contributions to the momentary viscous wall-shear stress  $\tau_w(t)$ .  $\langle u_d \rangle$  is compared with reference **horizontal r.m.s. fluctuation velocity**  $\sigma_U$ , where  $U = \sqrt{u^2 + v^2}_{\text{axis}}$  has been evaluated at the axis of a cylindrical sample [11]. In addition, **similarity functions**  $f_1$  [12] and  $f_2$  [13] for the streamwise r.m.s. fluctuation velocity  $\sigma_u$  from Blasius-type plate boundary layers (PBL) with matched  $Re_\tau \approx 2180$  are shown. All data sets are normalized by their individual maximum value. ODT and reference data exhibit the **inner peak**. A small **log region** is seen in ODT and DNS [11] that would emerge in  $f_2$  for larger  $Re_\tau$ . The **outer peak** ('shoulder') is less pronounced in present ODT results which is consistent with the transient PBL studied in [14].

- Fig. 3(d) shows the **r.m.s. deviation angle**  $\sigma_\gamma$  for  $\phi = \gamma$  denotes the local deviation angle,

$$\gamma(z, t) = \arctan\left(\frac{v(z, t)}{u(z, t)}\right) - \alpha_0(t),$$

which is measured between  $u_h = (u, v, 0)^T$  and  $e_d = (\cos \alpha_0, \sin \alpha_0, 0)^T$ . The deviation angle is small for  $z < \delta_U$  which supports the presence of a locally downstream-oriented Blasius-type surface layer.

- The thermal ( $\delta_T$ ) and viscous ( $\delta_U$ ) **boundary-layer thickness** have been obtained with the **slope method** (e.g. [11]) for  $\Theta$  (Fig. 3(a)) and  $\langle u_d \rangle$  (Fig. 3(c)), respectively. The shaded and hatched intervals give the **log-layer fitting ranges** used for ODT and DNS, respectively.

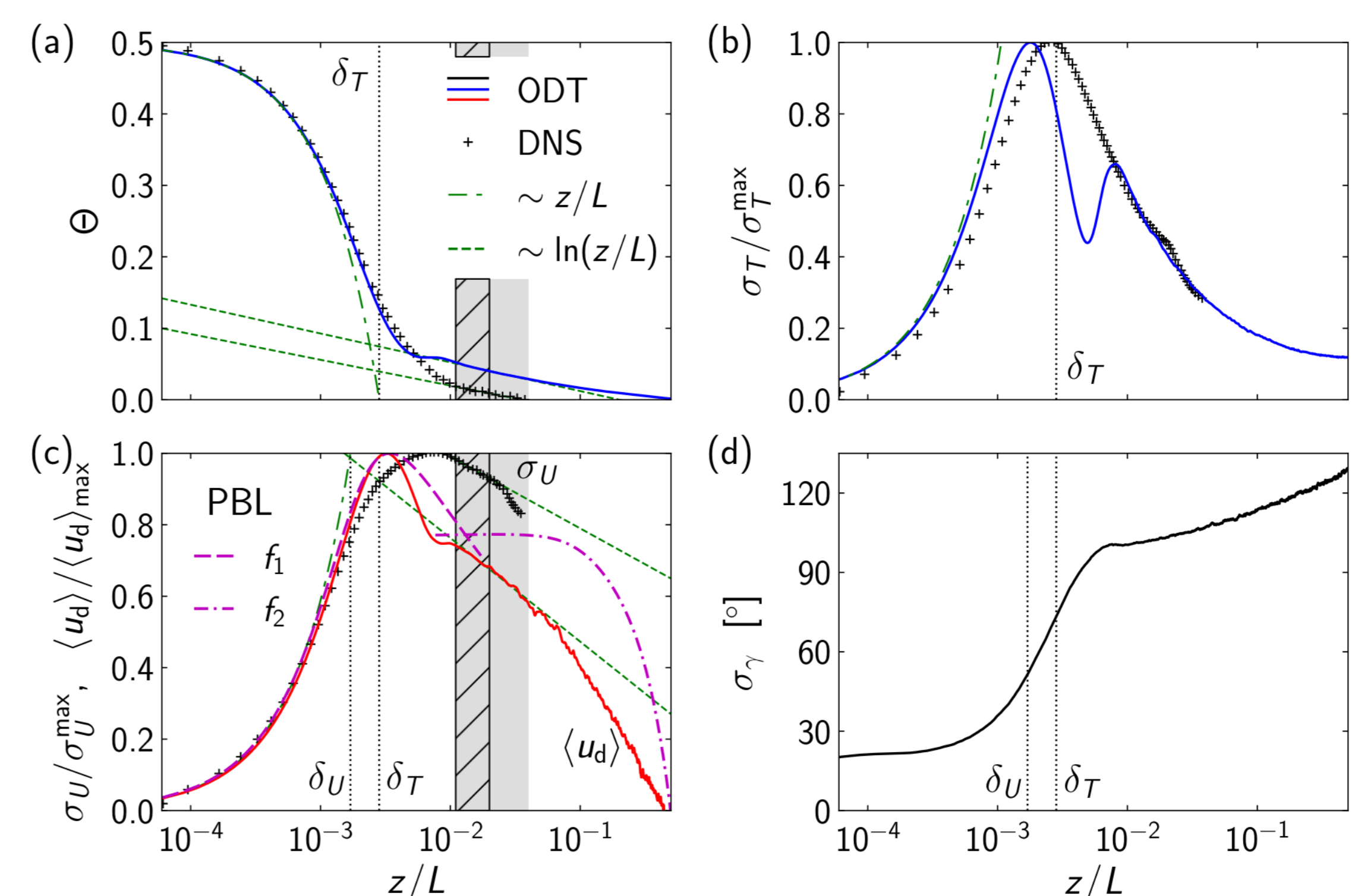


Figure 3: Thermal and viscous boundary-layer statistics in Rayleigh–Bénard convection for ODT and reference DNS [11]. (a) Normalized mean temperature  $\Theta$ . (b) Root-mean-square (r.m.s.) fluctuation temperature  $\sigma_T$ . (c) Boundary-layer 'downstream' velocity  $\langle u_d \rangle$  together with reference r.m.s. fluctuation velocity  $\sigma_U$  [11] and plate boundary-layer (PBL) r.m.s. similarity functions  $f_1$  and  $f_2$  [12, 13]. (d) ODT simulated r.m.s. deviation angle  $\sigma_\gamma$ . Thermal ( $\delta_T$ ) and viscous ( $\delta_U$ ) boundary-layer thicknesses are given for orientation. Log layers were fitted across shaded and hatched intervals.

## Conclusions

- **ODT** is a dimensionally reduced, **stochastic turbulence model** that aims to resolve the wall-normal (vertical) transport processes on **all relevant scales** of the flow.
- ODT exhibits **transient convective Blasius boundary layers** over the heated and cooled wall capturing relevant surface-layer fluctuation statistics.
- Local 'downstream' velocity conditional statistics exhibit the **inner peak**, which is well described by **plate boundary-layer similarity functions** [12, 13] for matched  $Re_\tau$ . The **outer peak** is weaker in ODT consistent with [14].

## References

- [1] F. Chillà, J. Schumacher, *Eur. Phys. J. E* **35**, 58 (2012).
- [2] J. Schumacher, V. Bandaru, A. Pandey, J. D. Scheel, *Phys. Rev. Fluids* **1**, 084402 (2016).
- [3] E. S. C. Ching, O.-Y. Dung, O. Shishkina, *J. Stat. Phys.* **167**, 626 (2017).
- [4] N. Shi, M. S. Emran, J. Schumacher, *J. Fluid Mech.* **706**, 5 (2012).
- [5] S. Grossmann, D. Lohse, *Phys. Fluids* **23**, 045108 (2011).
- [6] A. R. Kerstein, *J. Fluid Mech.* **392**, 277 (1999).
- [7] D. O. Lignell, A. R. Kerstein, G. Sun, E. I. Monson, *Theor. Comp. Fluid Dyn.* **27**, 273 (2013).
- [8] S. Wunsch, A. R. Kerstein, *J. Fluid Mech.* **528**, 173 (2005).
- [9] E. D. Gonzalez-Juez, A. R. Kerstein, D. O. Lignell, *Geophys. Astro. Fluid Dyn.* **107**, 506 (2013).
- [10] M. Klein, H. Schmidt, *Proc. 11th Int. Symp. Turb. Shear Flow Phen.* (Southampton, UK, 2019), vol. 1, pp. 1–6.
- [11] L. Li, et al., *Phys. Rev. E* **86**, 026315 (2012).
- [12] I. Marusic, A. K. M. Uddin, A. E. Perry, *Phys. Fluids* **9**, 3718 (1997).
- [13] I. Marusic, G. J. Kunkel, *Phys. Fluids* **15**, 2461 (2003).
- [14] Rakhi, M. Klein, J. A. Medina Méndez, H. Schmidt, *J. Turbul.* **20**, 506 (2019).